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IN THE SPECIFICATION: Please amend the specification as follows:

Page 2, lines 8 - 14

Another drawback is that because the wastewater solution is evaporated by a moving air stream, water droplets containing wastewater become suspended in the air, in addition to the clean water droplets. The humid air must then be treated with a demister to remove the water. This demister also ~~be comes~~ becomes contaminated with solids, causing decreased airflow, and must be periodically cleaned manually.

Page 3, lines 16 - 27

In an exemplary embodiment, the evaporator is a high temperature, flash type system, wherein a salt solution (brine) is circulated, under pressure, from a flash tank (e.g., at about 7 feet per second), through a heat exchange media, and back to the flash tank. As the brine circulates through the heat exchanger, its temperature increases to between about 220 to about 230°F (about 104 to about 110°C). The heated brine enters the flash tank via a fog nozzle, which induces a pressure drop. As a result of the pressure drop, the water mass transforms from liquid to vapor phase (i.e., the water evaporates to become steam) at rate determined by the amount of energy being introduced into the system. The steam is vented from the flash tank through a demister assembly. After the steam passes through the demister, it is introduced into an air stream for atmospheric venting or a secondary condensing operation to recover the water for reuse.

Page 6, lines 5 - 9

The flash ~~evaporator~~ tank (10) may continue to operate at the low limit level for a programmable length of time, e.g., six minutes, to compensate for foaming in the tank (10). As the brine begins to approach 215°F (102°C), flash evaporation occurs. As the fluid level in the tank drops, influent pump (22), and defoamer pump (20) cycle on and off to maintain the tank (10) level at the low-level limit.

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After the filter full signal is established, the filter inlet valve (41) closes and filter pump (44) turns off to stop influent flow. Blow down mode control valve (43) closes and shop air supply valve (48) opens to put the filter into blow down mode for a fixed period of time. Typically, in the preferred embodiment, blow down time is 10 minutes.

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After the filter blow down cycle has been completed, shop air valve (48) is closed, blown down control valve (43) is opened, and the filter press (38) hydraulics are started to open the filter. The filter press (38) is equipped with a system of chain and springs that link all of the filter plates together in order to automatically spread the filter plates as the press platen opens. The filter press is also equipped with a plate shaker system. When the filter platen reaches the full open position, a limit switch is energized and the filter press switches from plate open to plate shake mode. A hydraulic motor and cam attached to the filter press frame actuate to raise one side of the plates off the press frame rails then abruptly drop them, causing the solid cakes to separate and fall away from the press plates. The press remains in the shake mode for a programmable amount of time (for example 30 seconds). The solid is deposited directly into a receptacle suitable for landfill disposal of hazardous solids. No further handling of the solid cakes is necessary.

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The clean water purge of the system (8) continues until the flash evaporation tank (10) reaches the liquid low-level set point. When that tank reaches the minimum set point level, clean water valve (24) is turned off. The main circulation pump (12) is started and the system is allowed to wash itself with clean water for a programmable amount of time (typically 15 minutes) to allow any solids remaining in the system to dissolve back into solution.

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At the completion of the wash time, circulation pump (12) is turned off and all valves are closed. The cool down cycle indicator turns off and system control is returned to the manual control switches. The fresh water remains in the system (8) until the next evaporation cycle is started. When the next evaporation cycle is initiated, the fresh water is evaporated until the tank level control system calls for influent. This step heats the fresh water to approximately 230°F (110°C) at the beginning of the evaporation cycle. This superheated water is a very aggressive cleaner for the system that readily removes any scale deposits that may have formed on the heat exchange surfaces before the evaporation of the salt brine begins.

Abstract: Please replace the Abstract with the following paragraph:

One method for cleaning wastewater comprises: locating wastewater brine into a tank, circulating the brine under pressure through a heat exchange media; decreasing the pressure of the heated brine during re-introduction of the pressurized, heated brine by an amount effective to transform at least a portion of water from the brine from liquid to steam, and removing the steam from the tank.